

Plant CO<sub>2</sub> assimilation and O<sub>2</sub> after photosynthesis **OSMOSIS** like human from air **OSMOSIS** to organism.

Gradual reaction first pathway sequences start with water 12H<sub>2</sub>O flux from root to stomata cell membrane surface dissolve CO<sub>2(aqua)</sub> and Carbonic Anhydrase CA [CO<sub>2(aqua)</sub>]+[HCO<sub>3</sub><sup>-</sup>]=0.023 M from 400 ppm CO<sub>2</sub> air.

I) CO<sub>2(gas)</sub>+ΔG<sub>aqua</sub>⇌Q+CO<sub>2(aqua)</sub>; in endoergic ΔG<sub>Hydratation</sub>=10.77 kJ/mol and ΔH<sub>Hess</sub>=-20.3 kJ/mol solubility product:

K<sub>sp</sub>=[CO<sub>2(aqua)</sub>]/[CO<sub>2(gas)</sub>]/[H<sub>2</sub>O]=1/29.44=0.034045 endoergic ΔG<sub>sp</sub>=8.4 kJ/mol dissolve concentration:

$$[CO_{2(aqua)}]=K_{sp} \cdot [H_2O] \cdot [CO_2 \uparrow_{air}]=0.03397 \cdot 55.3457 \cdot 0.0004=1.878 \cdot 0.0004=0.0007537 \text{ M.}$$

II) Carbonic Anhydrase CO<sub>2(aqua)</sub>+2H<sub>2</sub>O+Q←<sup>CA</sup>→H<sub>3</sub>O<sup>+</sup>+HCO<sub>3</sub><sup>-</sup>←<sup>Membrane Channels</sup>→H<sub>3</sub>O<sup>+</sup>+HCO<sub>3</sub><sup>-</sup> improve carbon assimilation [HCO<sub>3</sub><sup>-</sup>]+[CO<sub>2(aqua)</sub>]=[HCO<sub>3</sub><sup>-</sup>]=0.0154 M+0.0076 M=0.023 M times 30.6=0.023 M / 0.0007537 M .

Produced protons and bicarbonate concentration gradient driving exoergic to Photosynthesis with HCO<sub>3</sub><sup>-</sup> , H<sup>+</sup>:



exoergic ΔH=-20.3 kJ/mol; endoergic ΔH=9.76 kJ/mol; athermic 0 kJ/mol; exoergic ΔH<sub>total</sub>= -10.54 kJ/mol;

endoergic ΔG<sub>sp</sub>=+8,4 kJ/mol; endoergic ΔG<sub>eq</sub>=+60 kJ/mol; exoergic ΔG<sub>channel</sub>= -10.62-7.48= -18.1 kJ/mol;

$$\Delta G_H=RT \ln([H_3O^+]_{right}/[H_3O^+]_{left})=8.3144 \cdot 298.15 \cdot \ln(10^{(-7.36)}/10^{(-5.5)})=-10.62 \text{ kJ/mol} \dots \dots \dots$$

$$\Delta G_{HCO_3}=RT \ln([HCO_3^-]_{right}/[HCO_3^-]_{left})=8.3144 \cdot 298.15 \cdot \ln(0.0007537/0.0154)=-7.48 \text{ kJ/mol} \dots \dots \dots$$

**HOMEOSTASIS** Norma bicarbonate concentration sum 0.023 M sustain multipurpose Attractor pH=7.36:

$$pH=pK_a+\log[HCO_3^-]/[CO_{2(aqua)}]=7.0512+\log(0.0154/0.0076)=7.36;$$

Pathways I), II) reach ENZYME complex Photo Synthetic Reaction Center (PRC) in **thylakoid cell**.



exoergic ΔH=6\*-10.54=63.24 kJ/mol and endoergic ΔG<sub>H3O+HCO3</sub>=ΔG<sub>sp</sub>+ΔG<sub>eq</sub>+ΔG<sub>channel</sub>=8.4+60-18.1=50.3 kJ/mol;

Second pathway start with 1) (PRC) Photo Synthetic Reaction Center ENZYME cluster of **green plants**.

PRC engine is **red** and **blue** light photons absorbed energy in glucose and one of 6 oxygen molecules to

calculate on one O<sub>2</sub> mole ΔH=2805.27/6=467.5 kJ/mol , ΔG=3049.55/6=508.3 kJ/mol. Sun radiation is consumed

also the heat energy drive evaporation **endoergic** of oxygen 6O<sub>2</sub> and water 6H<sub>2</sub>O out of **green plant** stomata

open hole. So aquaporins and evaporation substrates oxygen 6O<sub>2</sub> and water 6H<sub>2</sub>O increase osmotic pressure outside cell

1) C<sub>osm</sub>=6+6=12

C<sub>osm</sub>=1 C<sub>6H<sub>12</sub>O<sub>6</sub></sub>

11 times as osmolar: concentration in cell decreases from 12 to one

inside cell **PRC**

**E=hv PRC**

glucose C<sub>6H<sub>12</sub>O<sub>6</sub></sub> molecule and flow intensity through aquaporins

outside stomata

**light red blue**

increases pressure out of **green plant cells**. Pressure is proportional

hole

**photo synthesis**

to osmolar concentration difference ΔC<sub>osm</sub>=11\*X M eleven

6HCO<sub>3</sub><sup>-</sup>+6H<sub>3</sub>O<sup>+</sup>

BioEnergetic

C<sub>6H<sub>12</sub>O<sub>6</sub></sub>+6O<sub>2(aqua)</sub>+6H<sub>2</sub>O times X higher pressure π=ΔC<sub>osm</sub>•R•T kPa.

$$\Delta G_{Osmos}=RT \ln([O_{2(aqua)}]_{right}/[O_{2(aqua)}]_{left})=8.3144 \cdot 298.15 \cdot \ln(1/12)=-6.16 \text{ kJ/mol} \cdot 6 \cdot -6.16 = -36,96 \text{ kJ/mol for } 6O_2$$

$$\Delta G_{O_2}=RT \ln([O_2]_{right}/[O_2]_{left})=8.3144 \cdot 298.15 \cdot \ln(2.556 \cdot 10^{-4} \text{ M}/0.005 \text{ M})=-7.37 \text{ kJ/mol}; 6 \cdot -7.37=-44.2 \text{ kJ/mol for } 6O_2$$

$$\pi = 11 \cdot X \cdot R \cdot T \text{ kPa}; X=[C_6H_{12}O_6]=0,005 \text{ M}; \pi = 11 \cdot 0,005 \cdot R \cdot T=0,055 \cdot 8,3144 \cdot 298,15=136,3 \text{ kPa}$$

6O<sub>2</sub> and 6H<sub>2</sub>O through aquaporins pushed out of cells against twelve times higher gradient as reactants 1/12:

2) aquaporins H<sub>2</sub>O+O<sub>2(aqua)</sub>←<sup>Aquaporins</sup>→O<sub>2(aqua)</sub>+H<sub>2</sub>O ΔG<sub>Osmos</sub>=-6,16 kJ/mol exoergic 1/12 gradient athermic ΔH=0 :

$$0.005 \text{ M } H_2O+O_{2(aqua)} \xleftarrow{Aquaporins} O_{2(aqua)}+H_2O \Delta G_{O_2}=-7.37 \text{ kJ/mol exoergic gradient real athermic } \Delta H=0 :$$

$$\Delta G_{sum}=\Delta G_{Osmos}+\Delta G_{O_2}=-6.16-7.37=-13.53 \text{ kJ/mol osmosis and down along } O_2 \text{ gradient } 2.556 \cdot 10^{-4} \text{ M}/0.005 \text{ M.}$$

3) AIR 6O<sub>2(gas)</sub> 6H<sub>2</sub>O<sub>gas</sub> evaporation for one H<sub>2</sub>O+O<sub>2(aqua)</sub>+Q =>O<sub>2(gas)</sub>+ΔG+H<sub>2</sub>O<sub>gas</sub> endoergic , exoergic sum:

$$\Delta H_{H_2O}=44 \text{ kJ/mol}; \Delta H_{O_2}=11.75 \text{ kJ/mol}; \Delta G_{H_2O}=8.591 \text{ kJ/mol}; \Delta G_{O_2}=-77.55 \text{ kJ/mol};$$

$$\Delta G_{sum}=8.591-77.55=-68.96 \text{ kJ/mol} , \Delta H_{sum}=44+11,75=55.75 \text{ kJ/mol and Photosynthesis sum endoergic:}$$

$$\Delta G_{sumPRC}=-68.96-13.53+508.3=425.8 \text{ kJ/mol and } \Delta H_{sumPRC}=55.75+0+467.5=523.25 \text{ kJ/mol endoergic on } O_2:$$

$$\Delta G_{sumC_6H_{12}O_6}=6 \cdot 425.8=2554.8 \text{ kJ/mol and } \Delta H_{sumC_6H_{12}O_6}=6 \cdot 523.25=3139.5 \text{ kJ/mol} .$$

**Plants** need supply energy as heat to support **PRC** and evaporated products oxygen O<sub>2(gas)</sub> as well water

H<sub>2</sub>O<sub>gas</sub> vapor through stomata open hole. According Le Chatelier principle heat as energy supply shift

endoergic equilibrium evaporation of O<sub>2(gas)</sub> and H<sub>2</sub>O<sub>gas</sub> outside → through **green plant** stomata open hole.

Opening the stomata holes depends on environment temperature and humidity. Evaporation velocity increases at higher temperature as heat supply if at enough water supply usually from roots.

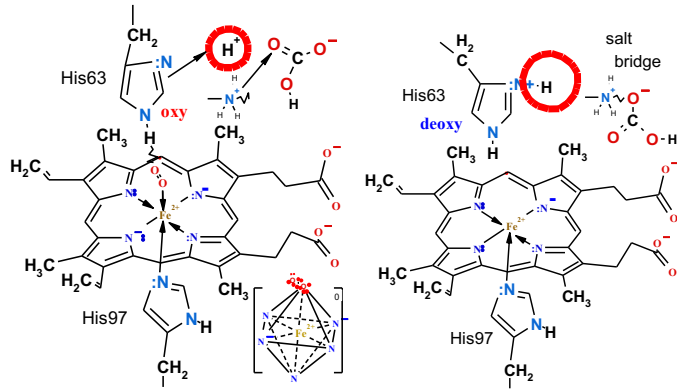
## Similar human O<sub>2</sub> OSMOSIS and oxidative assimilation with produced HCO<sub>3</sub><sup>-</sup> and CO<sub>2</sub> aqua

Reaction sequences start with root cells indispensable osmosis through membrane aquaporin channels.

I) **Oxygens** from AIR 20.95% O<sub>2</sub> dissolution in water by osmosis through aquaporins entrance in organism:

$\Delta H = -11.7 \text{ kJ/mol}$  exothermic  $\text{O}_{2\text{gas}} + \text{H}_2\text{O} \xleftarrow{\text{Aquaporin}} \text{H}_2\text{O} + \text{O}_{2\text{aqua}} + \text{Q}$   $\Delta G = 16.36 \text{ kJ/mol}$  endoergic.  $C_{\text{osm}} = 0.1 \text{ M}$  and soil  $C = 0.005 \text{ M}$   $\Delta G_{\text{O}_2} = RT \ln([\text{O}_{2\text{aqua}}]/[\text{O}_{2\text{gas}}]) = -8.3144 * 298.15 * \ln(0.1/0.005) = -7.426 \text{ kJ/mol}$  exoergic.

Plant **deoxy** Leghemoglobin **LHb<sub>T</sub>** from water medium adsorb inspired AIR O<sub>2</sub> aqua releases proton H<sup>+</sup>: **LHb<sub>R</sub>**(His63O<sub>2</sub>) + H<sup>+</sup> ← [O<sub>2</sub>] = 1.85 · 10<sup>-5</sup> M → (H<sup>+</sup>His63)**LHb<sub>T</sub>** + O<sub>2</sub> aqua and HCO<sub>3</sub><sup>-</sup>. In water solute oxygen



[O<sub>2</sub> aqua] = 9.768 · 10<sup>-5</sup> M concentration and average cytosolic value [O<sub>2</sub>] = 1.85 · 10<sup>-5</sup> M. Concentration gradient across membrane  $\Delta G_{\text{O}_2} = RT \ln([\text{O}_2]_{\text{right}}/[\text{O}_2]_{\text{left}}) = 8.3144 * 298.15 * \ln(1.85/9.768) = -4.125 \text{ kJ/mol}$ .

$\Delta G_{\text{sum}} = 16.36 - 7.426 - 4.125 = 4.809 \text{ kJ/mol}$ ,  $\Delta H_{\text{sum}} = -11.7 \text{ kJ/mol}$ .

II) pathway with carbonic anhydrase **AC** shifted to right by oxidative phosphorylation consume O<sub>2</sub> increase product HCO<sub>3</sub><sup>-</sup> and H<sup>+</sup> Leghemoglobin capturing (H<sup>+</sup>His63)**LHb<sub>T</sub>** stabilizes pH=7,36 concentration H<sub>3</sub>O<sup>+</sup>.

II)  $\text{Q}_{\text{aqua}} + \text{CO}_{2\text{aqua}} + 2\text{H}_2\text{O} \xleftarrow{\text{CA}} \text{H}_3\text{O}^+ + \text{HCO}_3^- \xleftarrow{\text{Membrane}} \text{H}_3\text{O}^+ + \text{HCO}_3^- \leftrightarrow \text{H}_2\text{O} + \text{H}_2\text{CO}_3 + \text{Q}_{\text{gas}} \leftrightarrow \text{H}_2\text{O} + \text{CO}_2 \uparrow_{\text{gas}} + \text{H}_2\text{O}$

endothermic  $\Delta H_{\text{H}} = +9.76 \text{ kJ/mol}$ ; athermic  $\Delta H_{\text{H}} = 0 \text{ J/mol}$  exothermic  $\Delta H_{\text{H}} = -9.76 \text{ kJ/mol}$ ; endothermic  $\Delta H_{\text{H}} = +20.29 \text{ kJ/mol}$ ;

gradient  $\Delta G_{\text{HCO}_3^-} = -RT \ln([\text{HCO}_3^-]_{\text{right}}/[\text{HCO}_3^-]_{\text{left}}) = -8.3144 * 298.15 * \ln((0.0154/0.0338919)) = -1.9554 \text{ kJ/mol}$ .

gradient  $\Delta G_{\text{H}_3\text{O}^+} = -RT \ln([\text{H}_3\text{O}^+]_{\text{right}}/[\text{H}_3\text{O}^+]_{\text{left}}) = -8.3144 * 298.15 * \ln((10^{-5.5}/0.02754)) = -22.49 \text{ kJ/mol}$ .

Sum  $\Delta G_{\text{Hess}} = \Delta G_{\text{HCO}_3^-} + \Delta G_{\text{H}_3\text{O}^+} = -1.9554 + -22.49 = -24.44 \text{ kJ/mol}$ ; endoergic  $\Delta G_{\text{Hess}} = 58.36 \text{ kJ/mol}$ ;

exoergic  $\Delta G_{\text{Hess}} = -22.44 \text{ kJ/mol}$ ; exoergic  $\Delta G_{\text{Hess}} = -58.205 \text{ kJ/mol}$ ;  $\Delta G_{\text{Hess}} = -8.538912 \text{ kJ/mol}$  exoergic.

Total sum in sequence **endothermic**  $\Delta H_{\text{Hess}} = +9.5876 + 0 - 9.76 + 20.291 = +20.1 \text{ kJ/mol}$  and free energy change

**exoergic**  $\Delta G_{\text{Hess}} = +58.36 - 22.44 - 58.205 - 8.538912 = -30.82 \text{ kJ/mol}$  spontaneous total sum in sequence.

Carbonic anhydrase make dominate buffer with protolysis constant  $\text{pK}_a = 7.0512$  on middle point:

$\text{CO}_{2\text{aqua}} + 2\text{H}_2\text{O} \xleftarrow{\text{CA}} \text{H}_3\text{O}^+ + \text{HCO}_3^-$ ;  $K_{\text{eq}} = [\text{H}_3\text{O}^+] \cdot [\text{HCO}_3^-] / [\text{CO}_{2\text{aqua}}] / [\text{H}_2\text{O}]^2 = 2.901 \cdot 10^{-11}$  is constant, but Brenstad protolysis constant with  $[\text{H}_2\text{O}] = 55.3 \text{ M}$  square  $K_a = K_{\text{eq}} \cdot [\text{H}_2\text{O}]^2 = [\text{H}_3\text{O}^+] \cdot [\text{HCO}_3^-] / [\text{CO}_{2\text{aqua}}] = 10^{-7.0512}$  forms its exponent  $\text{pK}_a = -\log(K_a) = 7.0512$ . Weak acid CO<sub>2</sub> aqua and HCO<sub>3</sub><sup>-</sup> is ubiquities buffer system in living organism.

The Attractor pH=7.36 reveals role of final product CO<sub>2</sub> aqua for **HOMEOSTASIS** reach the multipurpose Attractor value pH=7.36±0.01 according Henderson Haselbalh equation with alkaline reserve 2.0263=0.0154 M / 0.0076 M: **7.36=pH=pK<sub>a</sub> +log([HCO<sub>3</sub><sup>-</sup>]/[CO<sub>2</sub> aqua])=7.0512+log(0.0154 M / 0.0076 M)**.

CA carbon dioxide CO<sub>2</sub> aqua conversion to bicarbonate buffer processes endothermic  $\Delta H_{\text{Hess}} = +9.76 \text{ kJ/mol}$ , endoergic  $\Delta G_{\text{eq}} = +60 \text{ kJ/mol}$  create [HCO<sub>3</sub><sup>-</sup>] = 0.0154 M and [CO<sub>2</sub> aqua] = 0.0076 M concentrations. Consumed energy compensate exothermic and exoergic oxidation reactions produced energy and sun radiation absorbed heat and photon energy. Supplied energy is used to reach ENZYME clusters of Photo Synthetic Reaction Center (PRC) in **thylakoid cell** sustaining **HOMEOSTASIS** functional activity order with multipurpose Attractor value pH=7.36 as non equilibrium state:

Henderson Haselbalh expression  $\text{pH} = \text{pK}_a + \log([\text{HCO}_3^-] / [\text{CO}_{2\text{aqua}}]) = 7.0512 + \log(0.0154 / 0.0076) = 7.36$ ;

**O<sub>2</sub>, CO<sub>2</sub> metabolism, Carbonic Anhydrase, Shuttle deoxy-oxy LegHEMOGLOBIN  
CA Brønsted protolysis and hemoglobin shuttle enzyme of O<sub>2</sub>, HCO<sub>3</sub><sup>-</sup>+H<sup>+</sup>**

Enzyme **Carbonic anhydrase (CA)** protolysis multi functional **HCO<sub>3</sub><sup>-</sup>+H<sub>3</sub>O<sup>+</sup>** Attractor pH=7.36 .

**Shuttle** system, that stabilise **pH** at multi functional Attractor value **pH=7.36±0.01** despite the organism produces the metabolic **[CO<sub>2</sub><sub>aqua</sub>]=0.0275 M**. The **CA** made acidic products **[H<sub>3</sub>O<sup>+</sup>]=0.0275 M** are compensated by **shuttle** hemoglobin captured **H<sup>+</sup>+HCO<sub>3</sub><sup>-</sup>** after oxygen **[O<sub>2</sub><sub>aqua</sub>]=0.0275 M** desorbition due to oxidation product **CO<sub>2</sub><sub>aqua</sub>** in target cells of **tissues**:

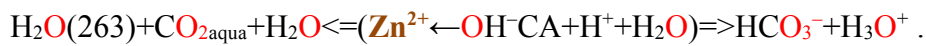
Hydrogen carbonate in human organism in amounts

**[HCO<sub>3</sub><sup>-</sup>]=0.0154 M, [CO<sub>2</sub><sub>aqua</sub>]=0.0076 M**, referring to

56.23 mL (50-60 mL) released volume **CO<sub>2</sub>** from 100 mL blood

as **alkaline reserve 2.036 / 1** in clinic evaluation.

Carbon dioxide forms by oxidation of carbohydrates, of fats and of proteins. Bicarbonate is created as product in hydration by CA enzyme **Zn<sup>2+</sup>** ion coordination center active site pocket:

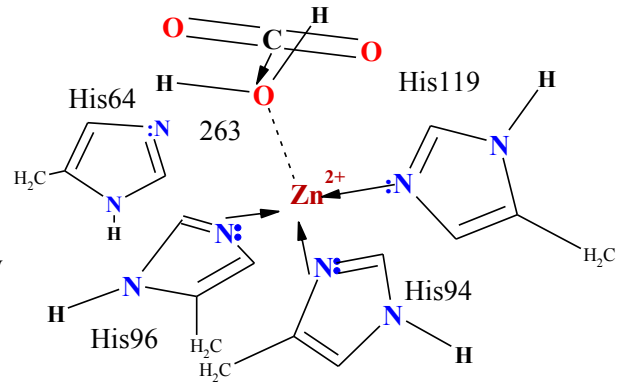


**H<sup>+</sup>+LHb<sub>R</sub>(His63O<sub>2</sub>)+HCO<sub>3</sub><sup>-</sup> ⇌ O<sub>2</sub><sub>aqua</sub>+LHb(H<sup>+</sup>His63)**...salt bridge..HCO<sub>3</sub><sup>-</sup> stabilizing concentration

**[O<sub>2</sub>]=6·10<sup>-5</sup> M**. **Deoxy** Leghemoglobin **LHb(H<sup>+</sup>His63)** capture proton **H<sup>+</sup>** at histidine residue and **HCO<sub>3</sub><sup>-</sup>** forms

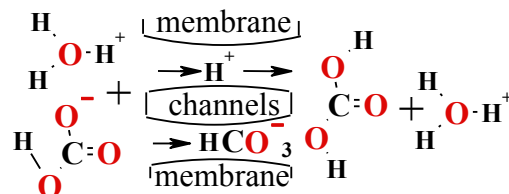
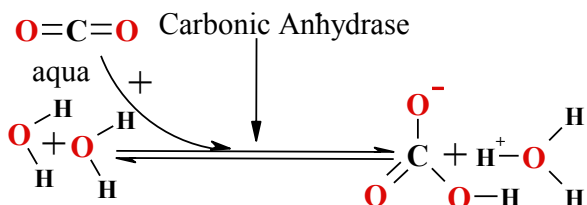
**deoxy LHb<sub>T</sub>(H<sup>+</sup>His63)**...salt bridge..HCO<sub>3</sub><sup>-</sup> (**Tense** state). In **thylakoid shuttle** Leghemoglobin absorbs oxygen

**oxy LHb<sub>R</sub>(His63O<sub>2</sub>) (Relax** state) and release proton **H<sup>+</sup>** , bicarbonate **HCO<sub>3</sub><sup>-</sup>** . From air 0.04 % **CO<sub>2</sub>**:



$2\text{H}_2\text{O} + \text{CO}_{2\text{gas}} \rightleftharpoons \text{CO}_{2\text{aqua}} + \text{Q}_{\text{aqua}} + \text{CO}_{2\text{aqua}} + 2\text{H}_2\text{O} \xleftarrow{\text{CA}} \text{H}_3\text{O}^+ + \text{HCO}_3^- \xleftarrow{\text{Membrane}} \text{H}_3\text{O}^+ + \text{HCO}_3^-$  and metabolic **CO<sub>2</sub><sub>aqua</sub>** exchanged with **O<sub>2</sub>** by ENZYME Carbonic Anhydrase (**CA**) convertes to **HCO<sub>3</sub><sup>-</sup>** , **H<sub>3</sub>O<sup>+</sup>** at stabilized pH=7.36±0.01 with **alkaline reserve 2.036/1**=[**HCO<sub>3</sub><sup>-</sup>**]/[**CO<sub>2</sub>**]=0.0154 M / 0.0076 M.

1) **first** reaction with ENZYME Carbonic Anhydrase (**CA**) converts oxidation product **CO<sub>2</sub><sub>aqua</sub>** , **2H<sub>2</sub>O** to bicarbonate anion. Multipurpose Attractor pH=7,36 create primary Attractor Carbonic Anhydrase CA:



2) **Second process** athermic  $\Delta H = 0 \text{ kJ/mol}$   $\text{H}_3\text{O}^+ + \text{HCO}_3^- \xleftarrow{\text{Membrane}} \text{H}_3\text{O}^+ + \text{HCO}_3^- + \Delta G$ ;  $\Delta G = -24.44 \text{ kJ/mol}$

exoergic gradients  $\Delta G_{\text{HCO}_3} = RT \ln([\text{HCO}_3^-]_{\text{right}}/[\text{HCO}_3^-]_{\text{left}}) = RT \ln((0.0154/0.0338919)) = -1.9554 \text{ kJ/mol}$ ; and

$\Delta G_{\text{H}} = RT \ln([\text{H}_3\text{O}^+]_{\text{right}}/[\text{H}_3\text{O}^+]_{\text{left}}) = RT \ln((10^{-5.5}/0.02754)) = -22.49 \text{ kJ/mol}$  where  $R = 8.3144 \text{ J/mol/K}$ ,  $T = 298.15 \text{ K}$ .

Transport ENZYMES catalyzes bicarbonate **HCO<sub>3</sub><sup>-</sup>** , proton **H<sup>+</sup>** move through membrane channels in **thylakoid**.

$[\text{O}_{2\text{aqua}}]=1.85 \cdot 10^{-5}$  M in *mitochondria* consumed for oxidation. Reactivity of  $\text{O}_{2\text{aqua}}$  cause desorption of  $\text{O}_{2\text{aqua}}$ :

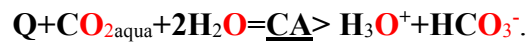


Oxygen through aquaporins crosses membrane into mitochondria. Concentration decreases below

$[\text{O}_{2\text{aqua}}]=1.85 \cdot 10^{-5}$  M. Each desorbed oxygen adsorbs one proton to distal histidine  $\text{H}^{\text{His63}}$  in LegHemoglobin  $(\text{H}^{\text{His63}})\text{LHb}_T$  and bind with salt bridge the  $\text{HCO}_3^-$ . So sustain  $[\text{HCO}_3^-]=0,0154$  M and  $[\text{CO}_{2\text{aqua}}]=0,0076$  M with alkaline reserve  $2.0263=0.0154 \text{ M} / 0.0076 \text{ M}$  according Henderson Haselbalh equation:

$7.36=\text{pH}=\text{pK}_a + \log([\text{HCO}_3^-]/[\text{CO}_{2\text{aqua}}])=7.0512+\log(0.0154 \text{ M} / 0.0076 \text{ M})$  and drive **HOMEOSTASIS** to keep the multipurpose Attractor value  $\text{pH}=7.36$  constant with concentration  $[\text{H}_3\text{O}^+]=10^{-7.36}$  M.

2)  $\text{CO}_{2\text{aqua}}$ , which is a product of metabolism comes from *mitochondria* and irreversible reacts with two water molecules **endothermic** cooling the environment, because consume the heat **Q**:



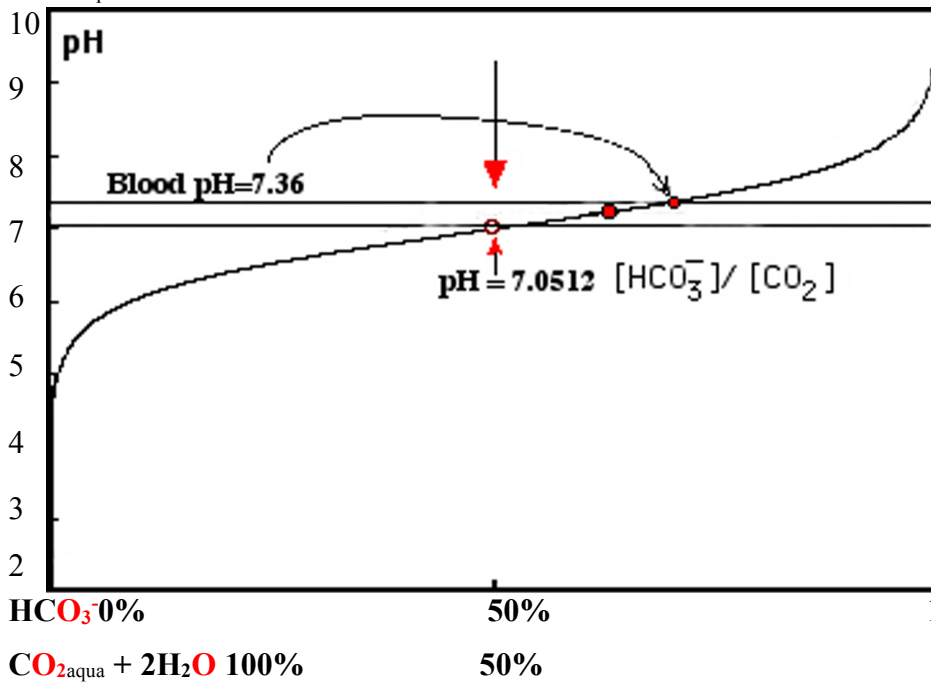
ENZYME Carbonic Anhydrase (CA) reaction shifts to right by heat **Q** supply, high water  $[\text{H}_2\text{O}]$  concentration 55.3 M, low hydroxonium ion concentration  $[\text{H}_3\text{O}^+]=10^{-7.36}$  M. The acid protolytic constant value  $\text{pK}_a=7.0512$  is friendly to multipurpose Attractor  $\text{pH}=7.36$  to prevent of carbonic dioxide accumulation, as CA Carbonic Anhydrase  $\text{CO}_{2\text{aqua}}$  converts to products  $\text{H}_3\text{O}^+ + \text{HCO}_3^-$ .

Green plants never evaporate  $\text{CO}_{2\text{aqua}}$  because Photosynthesis assimilate carbonic dioxide but in winter time at low temperatures stop the metabolism and did not produce the acid  $\text{CO}_{2\text{aqua}}$ . For animals buffer systems struggle with acidic products of metabolism final waste  $\text{CO}_{2\text{aqua}}$ , more and more of the acid form  $\text{CO}_{2\text{aqua}}$  of the buffer systems are produced. For this reason, the acid  $\text{CO}_{2\text{aqua}}$  have to be transported out of organism. For sustain of animal multipurpose Attractor  $\text{pH}=7.36$  endothermic evaporate  $\text{CO}_2 \uparrow_{\text{gas}}$ , or through kidneys membrane channels eliminate  $\text{H}_3\text{O}^+$  and  $\text{HCO}_3^-$ .

## Multipurpose Attractor pH=7.36 Henderson-Hasselbalh calculations

$$\frac{[\text{HCO}_3^-]}{[\text{CO}_{2\text{aqua}}]} = 10^{(\text{pH}-\text{pK})} = 10^{(7.36-7.0512)} = 10^{0.3088} = \frac{2.0263}{1}$$

the ratio  $[\text{HCO}_3^-]/[\text{CO}_{2\text{aqua}}]$  being approximately 2/1.



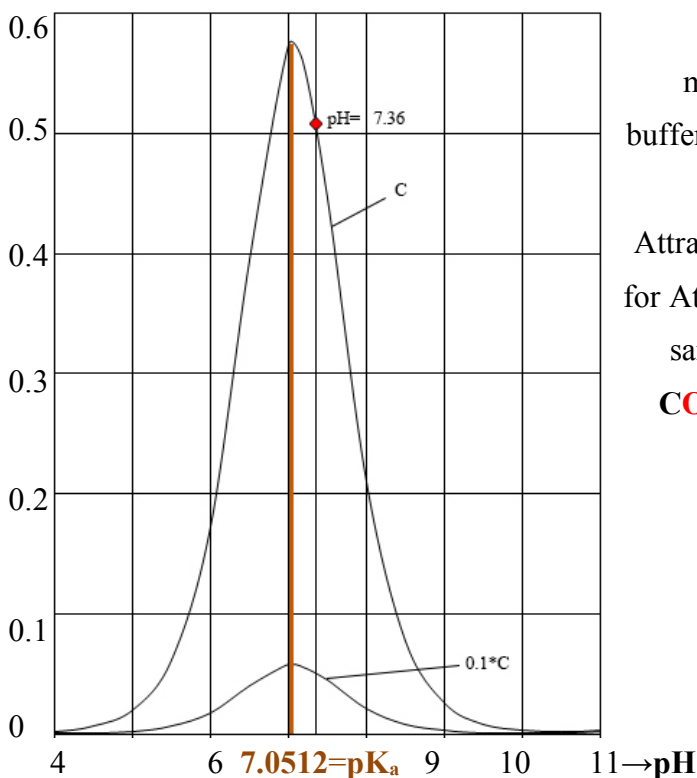
Buffer region middle point is the over inflection point in graph ○:  
 $\text{pH}=\text{pK}_a=7.0512$  as ratio  $[\text{HCO}_3^-]/[\text{CO}_{2\text{aqua}}]=1$  is one as well buffer component concentrations are equal  $[\text{HCO}_3^-]=[\text{CO}_{2\text{aqua}}]$ . Bicarbonate protolytic base  $[\text{HCO}_3^-]$  concentration is equal to Brensted acid  $\text{CO}_{2\text{aqua}}$  concentration  $[\text{CO}_{2\text{aqua}}]$ .

Alkaline reserve at  $7.36=\text{pH}$  is physiologic **Norma** and ratio is

$$\frac{[\text{HCO}_3^-]}{[\text{CO}_{2\text{aqua}}]} = \frac{0.0154 \text{ M}}{0.0076 \text{ M}} = \frac{2.0263}{1}$$

If  $\text{H}^+$  concentration grows Carbonic Anhydrase equilibrium is shifted to left and  $\text{CO}_2$  transported out as  $\text{H}^+$  with  $\text{HCO}_3^-$  by respiration through *stomata* spongy mesophyll cell surface and acid concentration  $[\text{H}^+]$  decreases. If concentration  $\text{H}^+$  decreases, Carbonic anhydrase equilibrium is shifted to the right and the extra amount of  $\text{HCO}_3^-$  through *stomata* cell surface passes transported out. Bicarbonate channels in *stomata* spongy mesophyll cell surface are open at values of  $\text{pH}=7.36$  and higher from inside of cytosol circulation, but are open to outside at low values perhaps proposed  $5 < \text{pH} < 7.36$  for cytosol  $\text{HCO}_3^-$  bicarbonate evaporation out to air as  $\text{CO}_2$  form.

$\beta$ , eq.mol/L buffer capacity .



The  $\text{pK}_a=7.0512$  of protolytic acid constant is friendly to multipurpose Attractor  $\text{pH}=7.36$ . Acidic in organism has to buffering with reserve of alkalinity. Therefore the ratio between  $\text{HCO}_3^-$  and  $\text{CO}_2$  concentrations is 2/1 and the  $\text{pH}$  value of Attractor is 7.36. *The alkaline reserve*  $2.036/1=[\text{HCO}_3^-]/[\text{CO}_2]$  for Attractor  $\text{pH}=7.36$  is controlled by adding  $\text{H}_2\text{SO}_4$  to 100 mL sample ( $\text{H}_2\text{SO}_4$  reacts with  $\text{HCO}_3^-$  and the  $\text{CO}_{2\text{aqua}}$ , liberated  $\text{CO}_2$ ). If 56.23 mL of gaseous  $\text{CO}_2$  are liberated, the *alkaline*

*reserve* in **homeostasis** is **norma** and total amount concentration  $0.023\text{M}=[\text{HCO}_3^-]+[\text{CO}_2]$  is of  $[\text{HCO}_3^-]=0.0154 \text{ M}$  with  $[\text{CO}_2]=0.0076\text{M}$ .

